

LOR Crude unit 1 APC

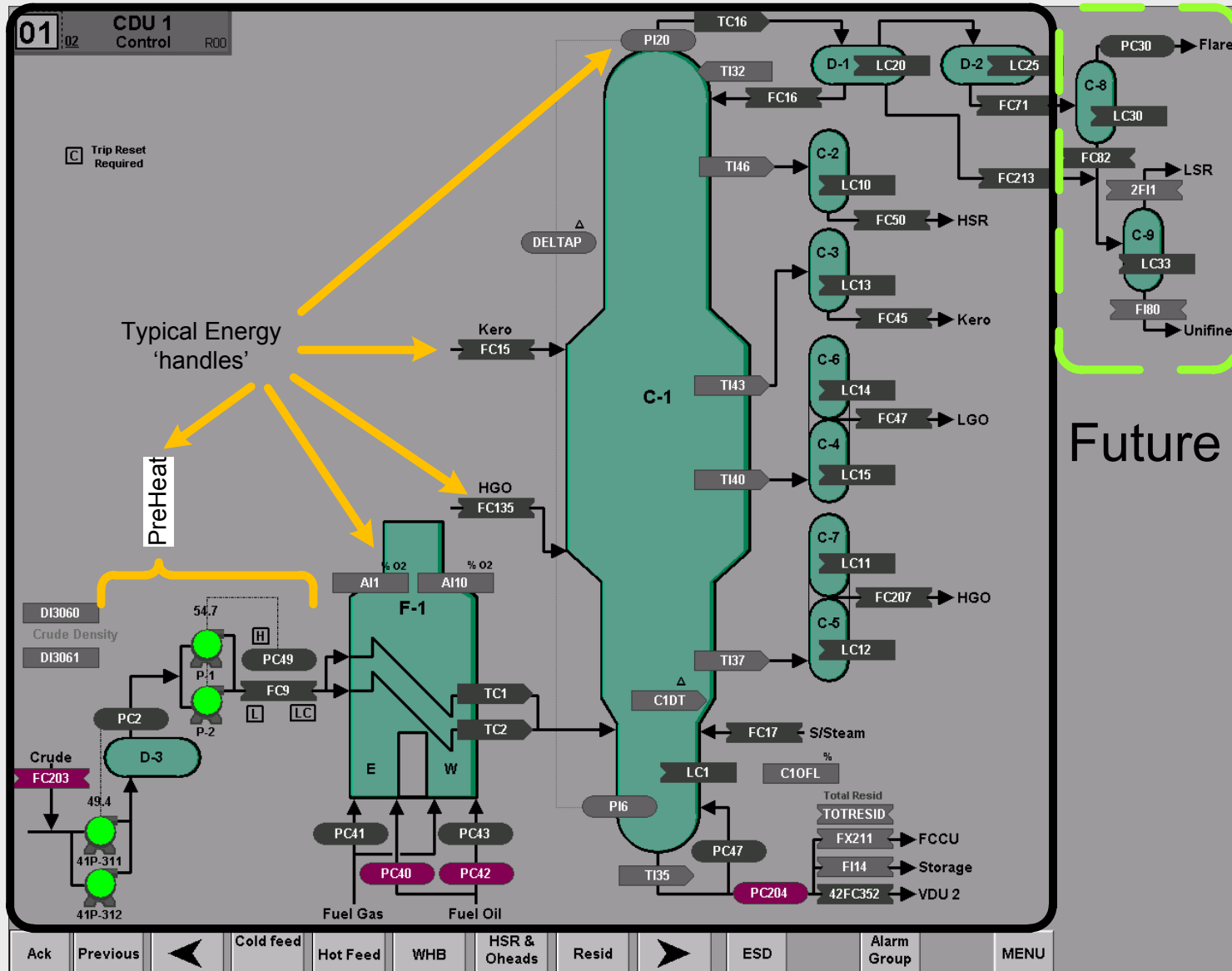
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Laurent Ferrari
Sean Goodhart
Barry Rutter
Zak Friedman

Agenda

- **Process APC description and scope**
- **Multivariable predictive controller**
- **Inferential models**
- **Issues with Inferential ‘trust’ versus analyzer readings and Lab**
- **Energy on CDU and APC projects**

LOR CDU1 APC scope



Future scope

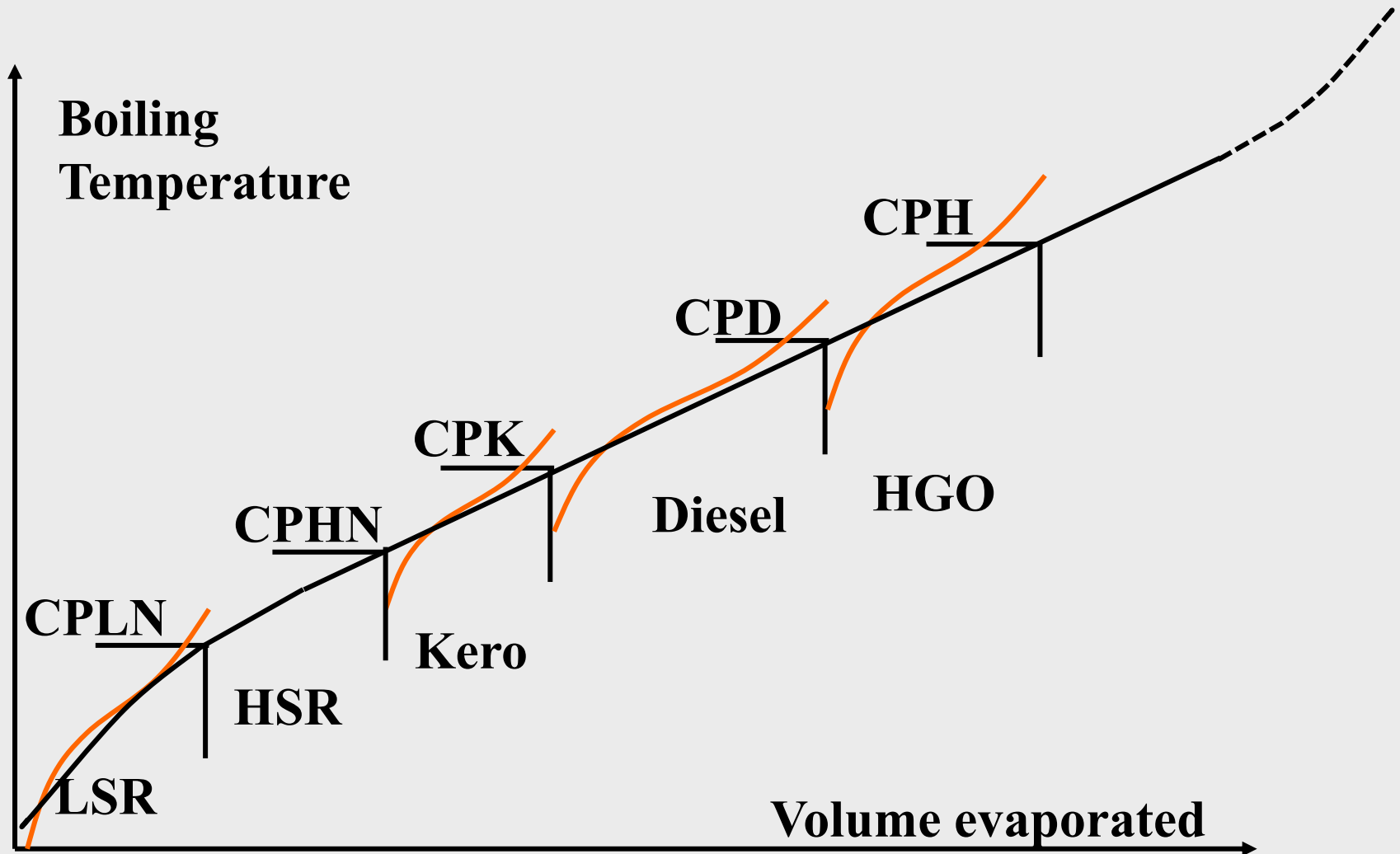
APC considerations

- **CDU is the first refinery unit and correctly splitting the crude oil at that stage is a must for a better overall refinery performance.**
- **Hence CDU APC is lucrative. It works via**
 - **Inferential models**, estimating the many product qualities (distillation and cold properties).
 - **MVPC**, pushing the unit continuously against plant constraints and product specifications.
- **Quality inferences are key to successful APC. They must perform well at all times:**
 - **Whatever the crude slate or type**
 - **Whatever the type of spec to run with**

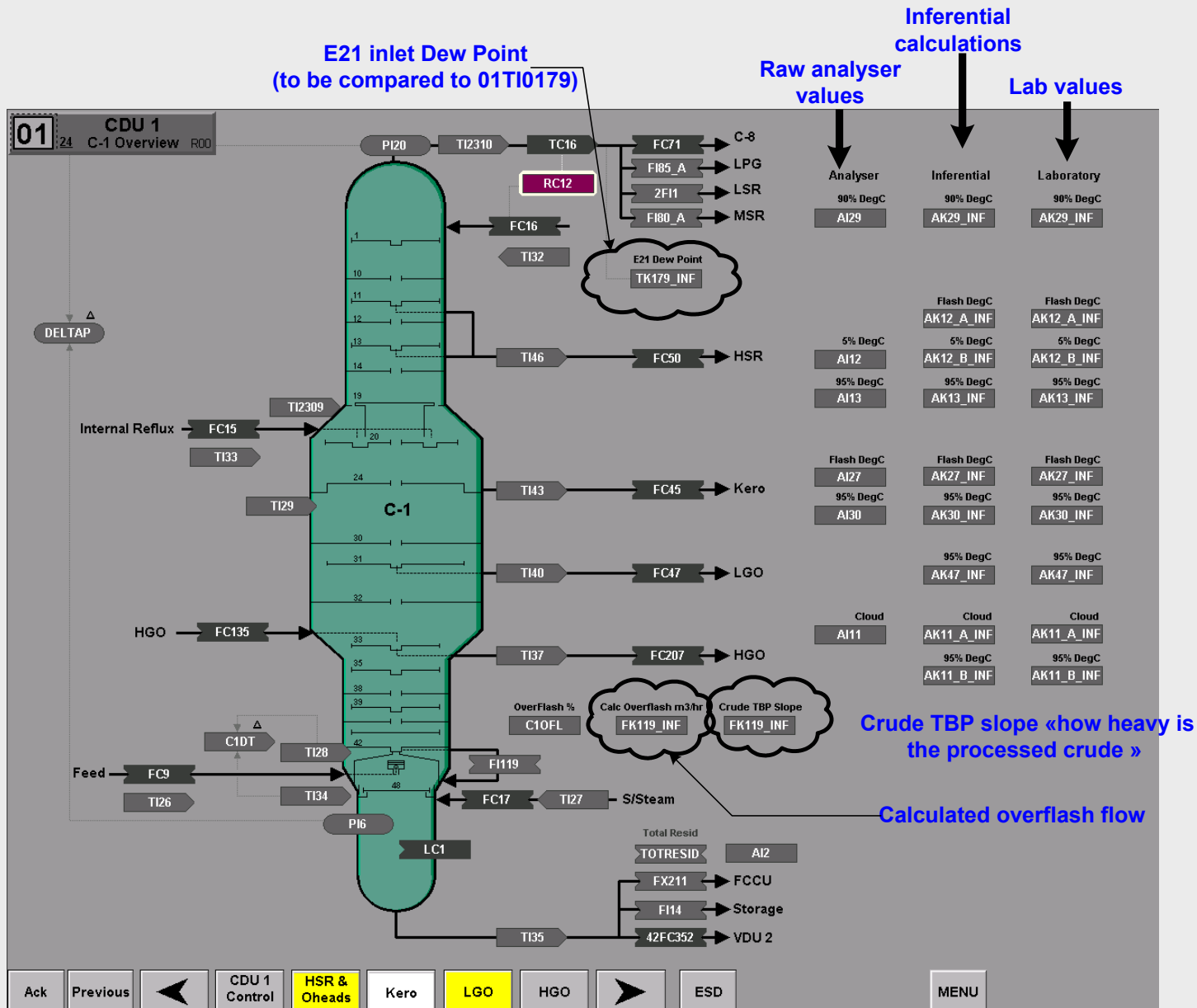
Inferential model methodology

- **A calculation based on “field measurements” such as flows, pressures, temperature.**
 - These calculations are based on thermodynamics first principles
 - A TBP (true boiling point) curve of the crude is estimated from column conditions
 - Internal reflux flows, including the most important over-flash flows are also estimated
 - From that information the model calculates all the different product properties (Flash, 5%, 95%, etc.)

Estimate the crude TBP curve



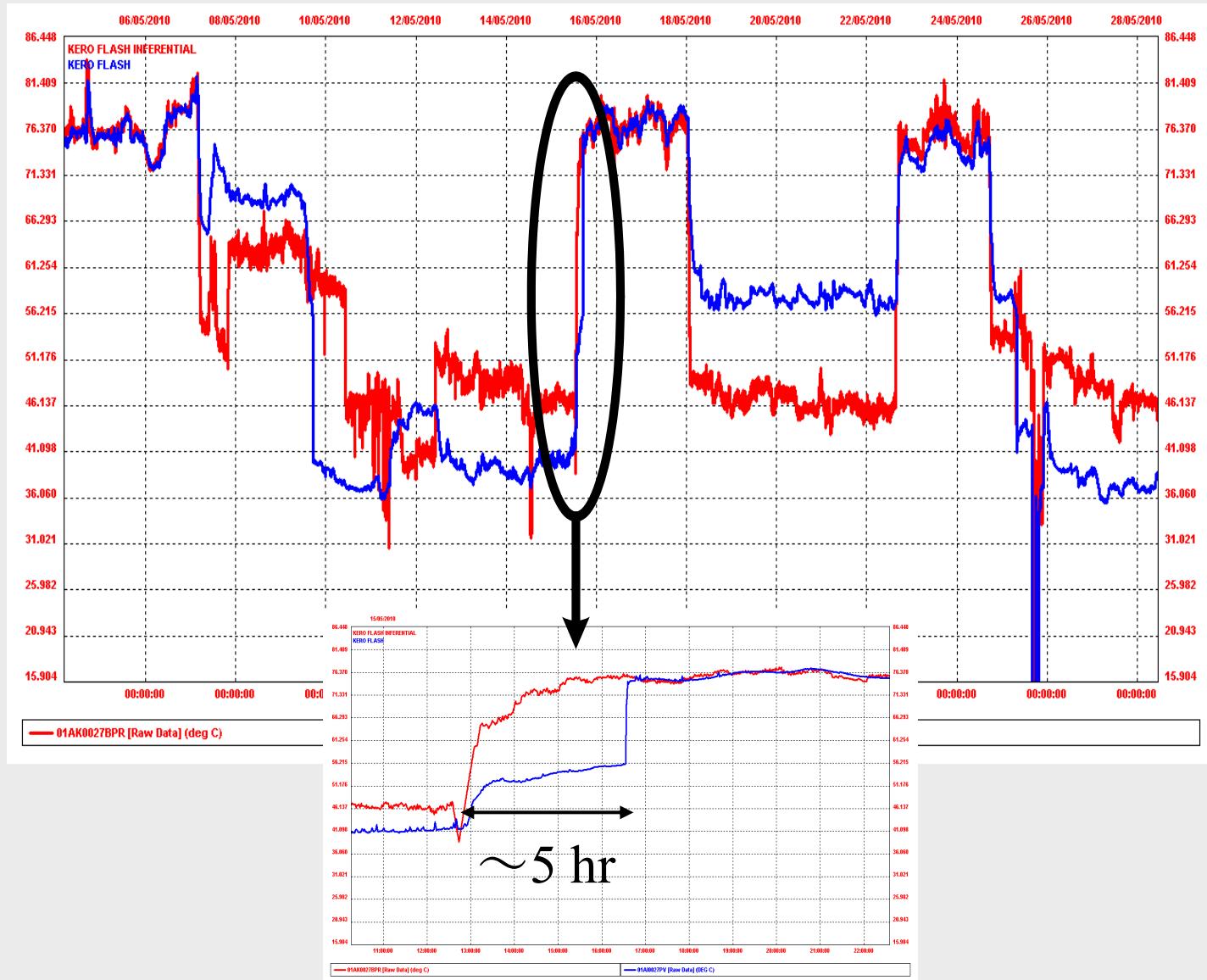
LOR inferences



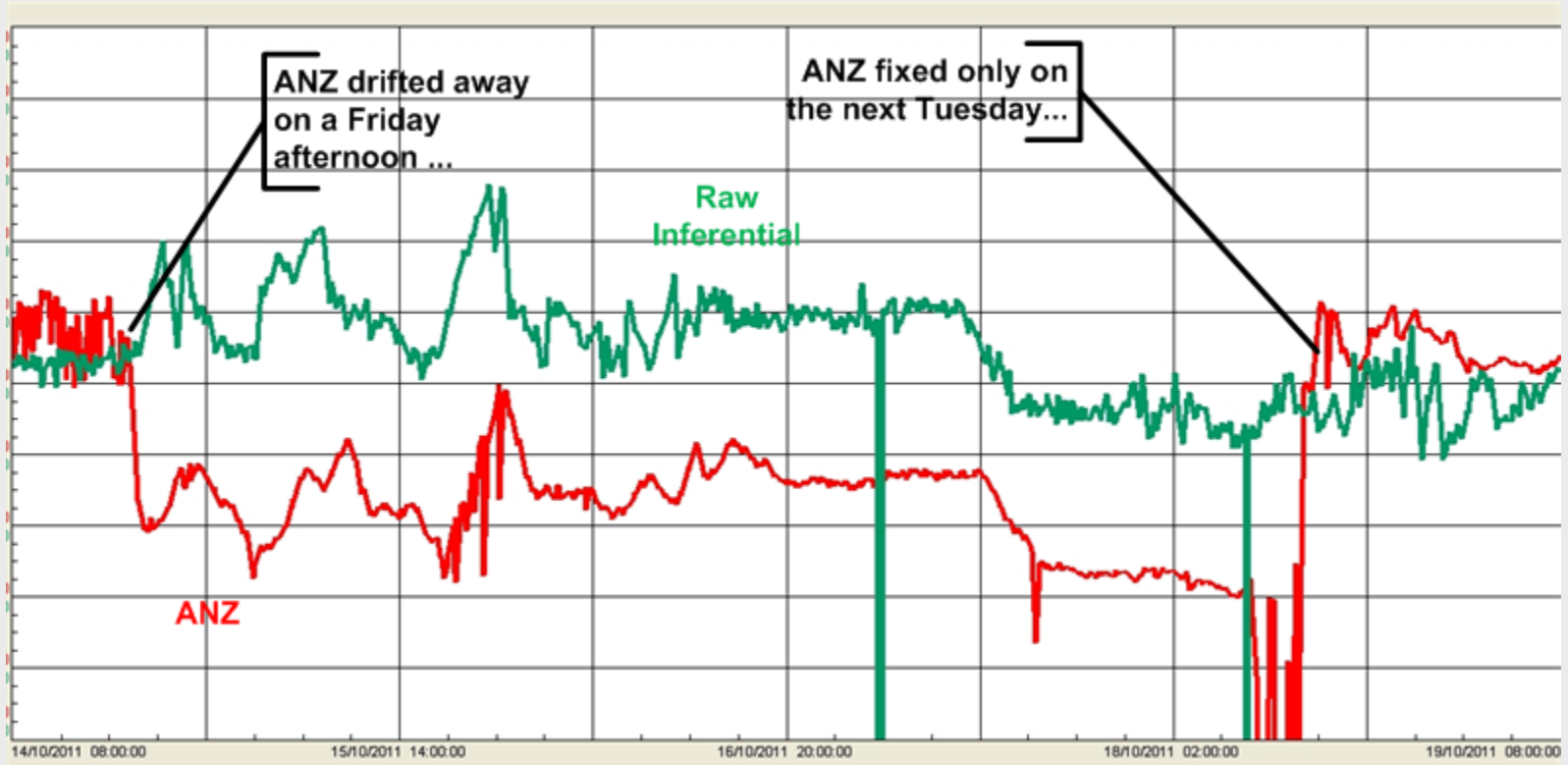
Inference versus analyzer

- **Analysers are slow by nature, not giving the right speed of results for fast control actions when needed.**
- **Also during a specification product transition, the analyzer **takes time to line up to the new product.****
 - **Operators do not believe the analyser as it takes 5 hours to switch properly (change of measurement method requires a switch on the analyser)**
 - **They wait for a Lab value to come ... which takes time as well ...**
 - **The inferential is there at all time. If it generally agrees with the lab it becomes quite useful**

Inference versus analyzer trend 1



Inference versus analyzer trend 2

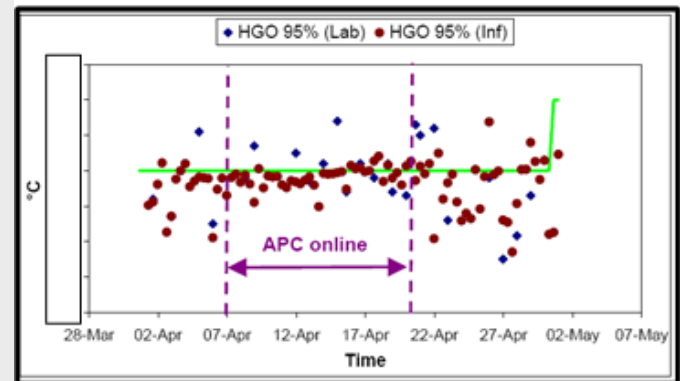
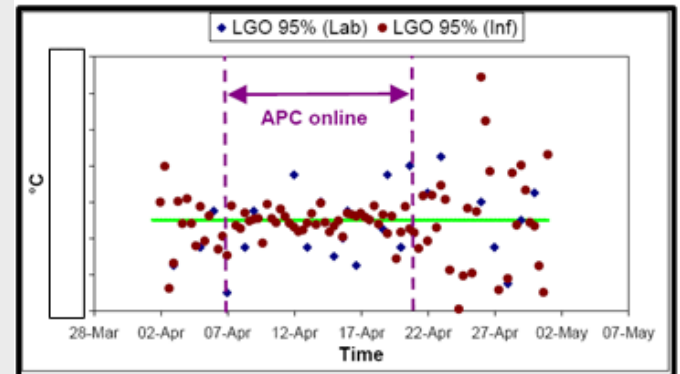
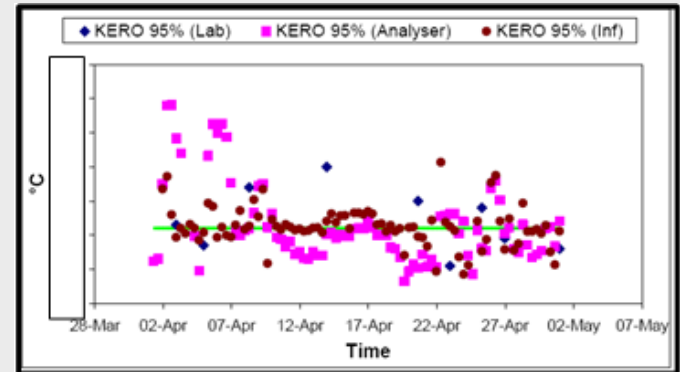


CDU APC strategy

- **Control product qualities to targets given by the planers, in order to optimally feed downstream units**
- **Push the feed rate up to:**
 - Requested production target
 - Approach but do not exceed unit constraints
- **Reduce the time of crude switches**
- **Handle the different production modes ('specialities' for Kerosene)**

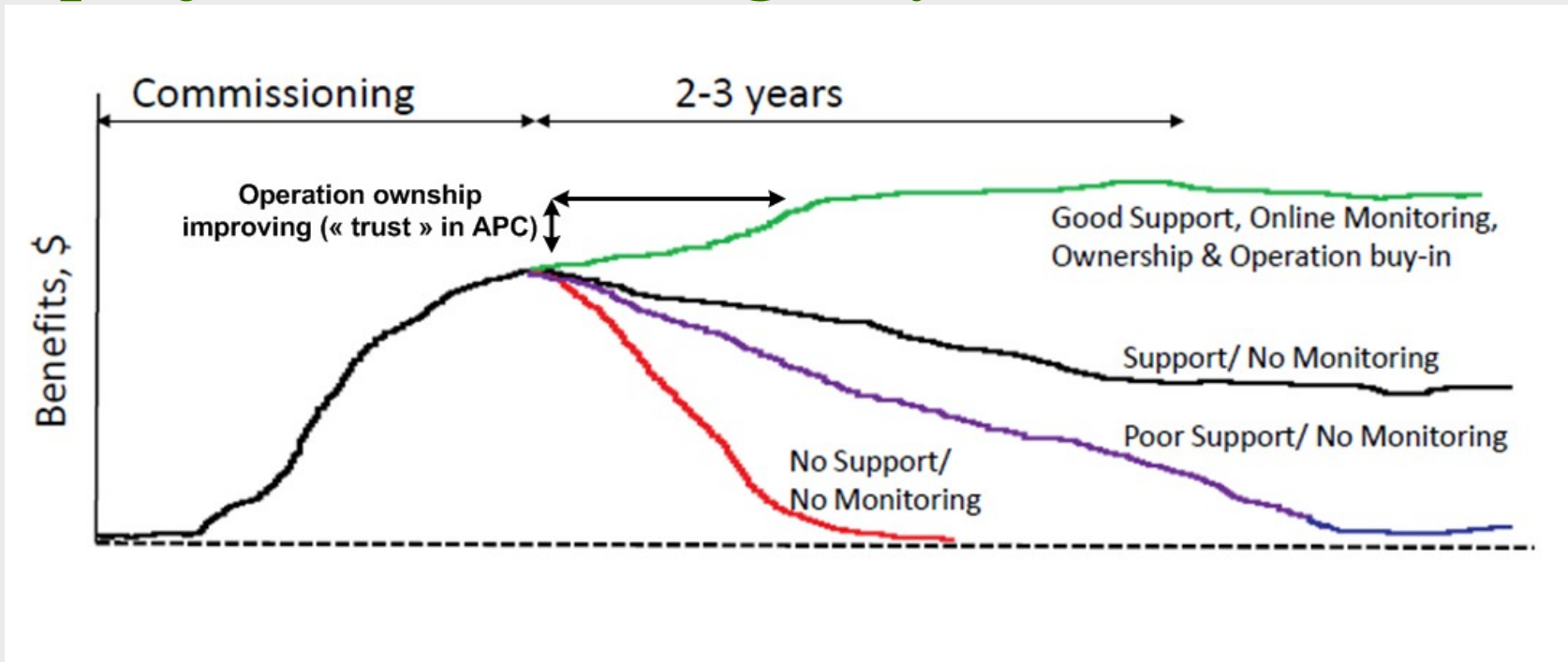
Benefits

- **First of all, a high operator acceptance and trust with a typical service factor over 85%, up to 99%**
- **Financial benefits > 6 M€/y (due to higher distillate recovery)**



After the project

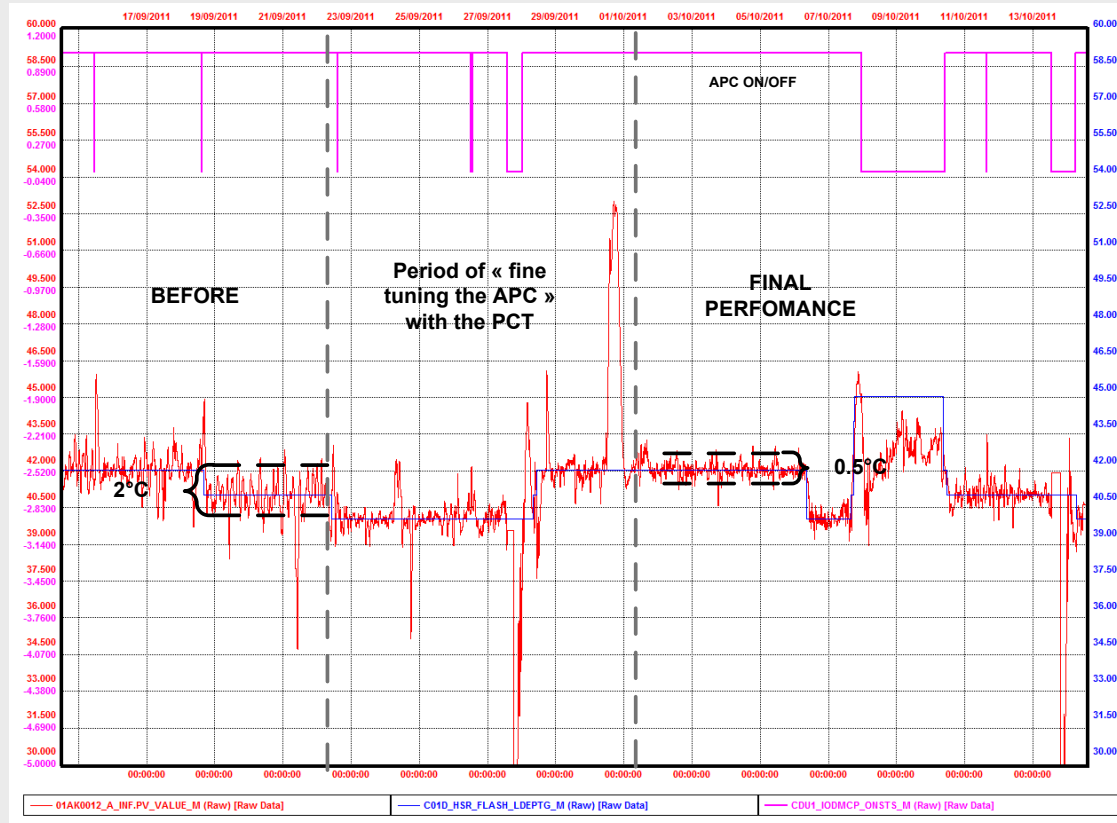
- We often speak about successful APC project and how long they can last ‘alive’...



- The APC project cannot capture all the APC potential benefits and continuous improvement is a must.

After the project improvement

- HSR Flash point control improved over time:
 - Standard deviation reduced by a factor of 4.
 - Benefits: 90k\$/m



Energy optimization

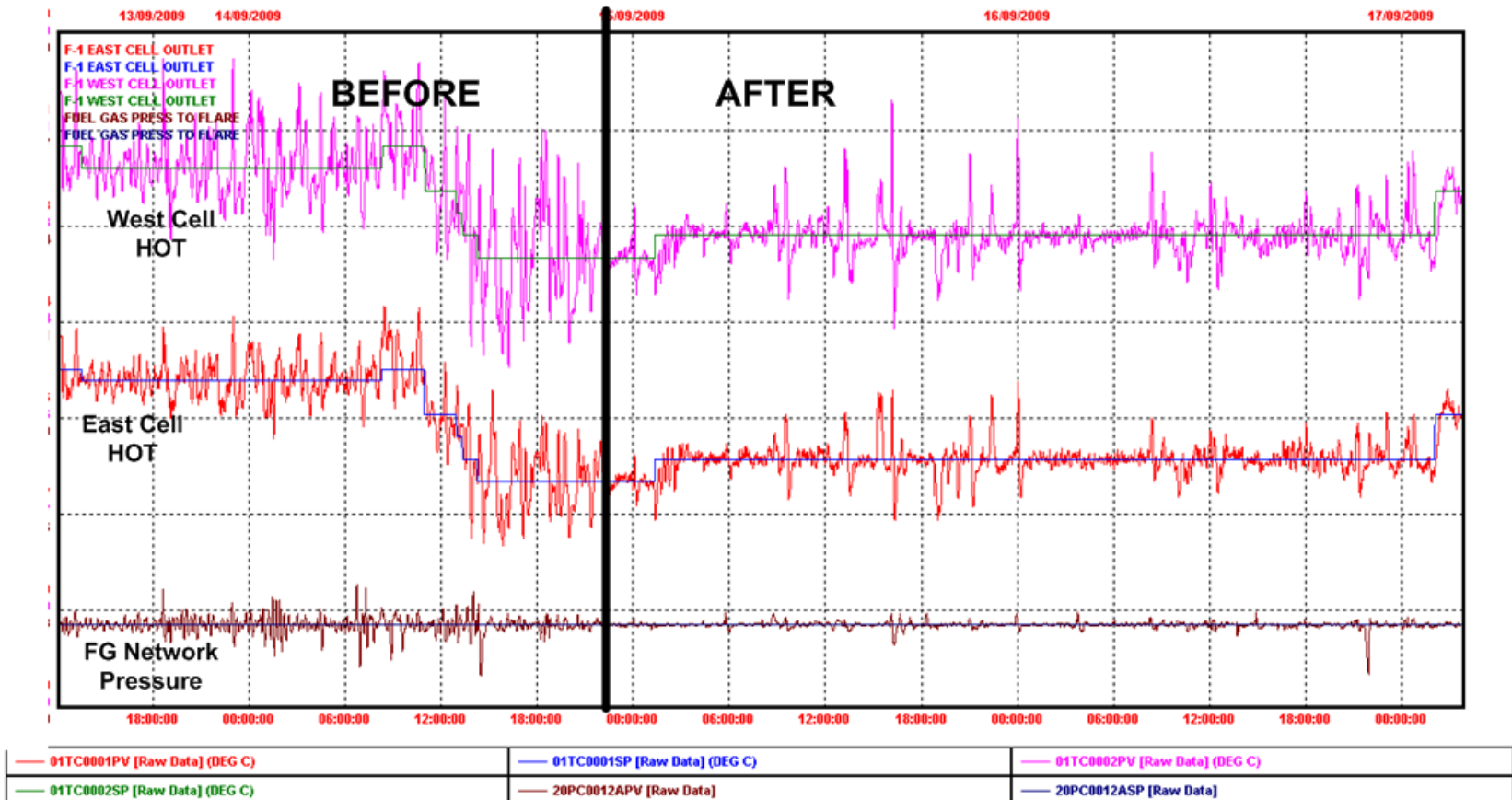
- **The trade-offs among throughput, yields and fuel consumption are studied off line to establish energy related targets**
 - Preheat system flow splits
 - Pumparounds heat duty splits
 - Heater outlet temperature
 - Stripping steam ratios
- **APC drives the plant towards these targets.**

Heater control

- **The large CDU heater must be stabilized and optimized or else entire APC objective is in jeopardy.**
- **Once that is accomplished we desire to minimize furnace excess air to environmental constraints.**
 - **Improvement of the Fuel gas network**
 - **Improvement of the Heater Outlet Temperature control**
 - **Improvement of the heater flue Gas O₂ control**

Furnace COT control

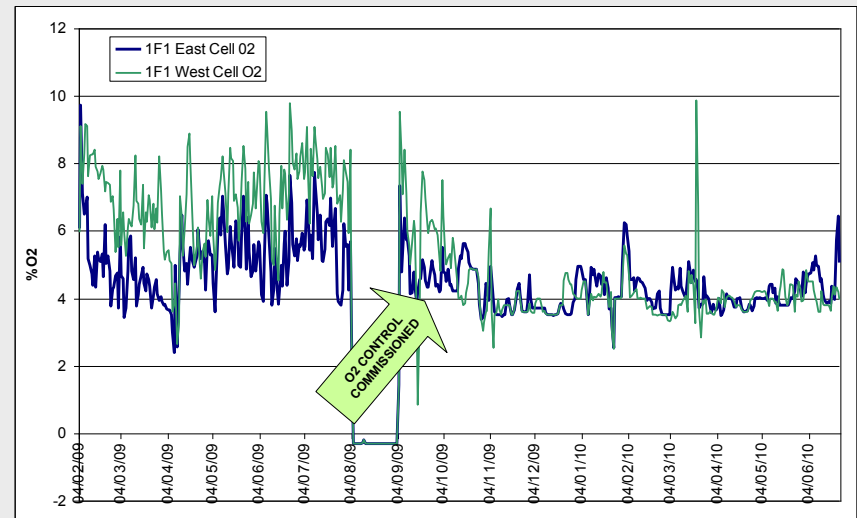
A first step of better usage of energy on the heater: stabilize heater operation (leading to better product separation)



Furnace stack O₂ control

The second step is to optimise the furnace efficiency using a stack O₂ control. The benefits: 195k\$/y.

- Previous improvement already stabilise stack O₂ (green curve).
- Now the O₂ control is made available to further improvements and energy benefits.



Conclusions

- **This is APC at its best**
 - **Controlling product properties at targets**
 - **Controlling internal reflux at reasonable targets**
 - **Keeping the unit within constraints and if that is not possible – cut throughput**
 - **Reducing the chance of incidents by handling crude switches smoothly**
- **TOTAL estimates the CDU APC benefits at > 6 million Euro/annum**